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Nicolas Frangieh, Dominique Morvan, Sofiane Meradji, Gilbert Accary, Oleg Bessonov. Numerical simulation of grassland fires behavior using an implicit physical multiphase model. Fire Safety Journal, 2018, 102, pp.37-47. 10.1016/j.firesaf.2018.06.004 . hal-02114073

HAL Id: hal-02114073 https://amu.hal.science/hal-02114073v1

Submitted on 29 Apr 2019

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Accepted Manuscript

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PII: S0379-7112(18)30037-7

DOI: 10.1016/j.firesaf.2018.06.004

Reference: FISJ 2718

To appear in: Fire Safety Journal

Received Date: 29 January 2018

Accepted Date: 18 June 2018

Please cite this article as: N. Frangieh, D. Morvan, S. Meradji, G. Accary, O. Bessonov, Numerical Simulation of Grassland Fires Behavior Using an Implicit Physical Multiphase Model, *Fire Safety Journal* (2018), doi: 10.1016/j.firesaf.2018.06.004

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Numerical Simulation of Grassland Fires Behavior Using an Implicit Physical Multiphase Model

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Abstract

12 This study reports 3D numerical simulations of the ignition and the propagation of 13 grassland fires. The mathematical model is based on a multiphase formulation and on a 14 homogenization approach that consists in averaging the conservation equations (mass, 15 momentum, energy ...) governing the evolution of variables representing the state of the 16 vegetation/atmosphere system, inside a control volume containing both the solid-17 vegetation phase and the surrounding gaseous phase. This preliminary operation results 18 in the introduction of source/sink additional terms representing the interaction between 19 the gaseous phase and the solid-fuel particles. This study was conducted at large scale in 20 grassland because it represents the scale at which the behavior of the fire front presents 21 most similarities with full scale wildfires and also because of the existence of a large 22 number of relatively well controlled experiments performed in Australia and in the 23 United States. The simulations were performed for a tall grass, on a flat terrain, and for 24 six values of the 10-m open wind speed ranged between 1 and 12 m/s. The results are in 25 fairly good agreement with experimental data, with the predictions of operational 26 empirical and semi-empirical models, such as the McArthur model (MK5) in Australia and 27 the Rothermel model (BEHAVE) in USA, as well as with the predictions of other fully 3D physical fire models (FIRETEC and WFDS). The comparison with the literature was 28 29 mainly based on the estimation of the rate of fire spread (ROS) and of the fire intensity, 30 as well as on the analysis of the fire-front shape.

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10 11

Keywords: Grassland fires, fire modeling, turbulent reactive flows, numerical simulation,
 high performance computing.

34 **1. Introduction**

35 Wildfire can be considered as a natural disaster or a necessary perturbation in the life of an ecosystem, depending on the place where this event occurs and on its intensity. The 36 37 frontier between these two points of view depends strongly on the impact of this event 38 on the environment and the economy, as well as on the management and the land use 39 between natural and urban areas[1]. The ecologists often consider that the existence of 40 low intense fires in natural areas (such as the national parks) is necessary to maintain 41 locally the biodiversity, whereas many citizens can consider them as an unsupportable 42 degradation of the environment, assimilated here as a recreation area. The fire regime, 43 defined by integrating a set of characteristic parameters of fires (patterns, intensity, and 44 frequency) for which an ecosystem presents an optimum resilience, is a good indicator of 45 the level of perturbation caused by external factors such as climate changes or the level

46 of anthropization [2]. Various factors have in the past and can in the future, cause great 47 modifications in the fire regime in a local area, such as the European settlement in 48 America, in Australia, and in other parts of the world, the rural exodus, and global 49 warming [3]. These changes can be particularly dramatic, when very intense fires occur 50 in the wildland-urban interface (WUI) as it happened in Victoria state in Australia in 2009 51 (Black Saturday) [4] and more recently in 2016 in Alberta (Canada) near the city of Fort 52 McMurray. To have an idea of the level of destruction of such "natural" hazard (a lot of 53 fire ignitions have human caused), one of the fires occurring during the "Black Saturday" 54 event (the Kilmore East fire), had burnt more than 125 000 ha of forest, tree plantations 55 and shrubs (100 000 ha in less than 12 hours), had caused 232 casualties (and 119 56 injuries), and had destroyed 1242 houses [4,5]. The fireline intensity was evaluated to 57 88 000 kW/m (in comparison, the average power of a unit in a nuclear power plant is 58 about 1500 MW) [3].

59 Due to the extreme complexity of the problem, most of operational tools predicting 60 wildfires behavior (such as PHOENIX [6] in Australia and FARSITE in USA [7]) are based 61 on statistical or semi-empirical approaches, namely the MacArthur MK5 model [8,9] in 62 Australia and the Rothermel model (BEHAVE) in USA [10]. However, in many situations, especially that deviate from the conditions on which these models were calibrated, the 63 quality of the predictions compared to real observations collected on well documented 64 65 fire can be qualified as poor [11]. These tools propose to evaluate some characteristic parameters of fire, such as the rate of spread (ROS), the fire intensity, and the flame 66 height. However, the validity of the predictions of empirical models are limited to the 67 range of parameters used to develop the statistical laws. As for semi-empirical models, 68 69 such as BEHAVE, predictions at large scale are of poor quality because most of them are 70 made by extrapolation of data obtained from small-scale fires performed in a wind tunnel 71 through homogeneous dead fuel bed (pine needles, excelsior, sticks) [11], which may lead 72 sometimes to unexpected results such as a ROS greater than the wind speed. Such 73 behavior cannot be explained physically, except in the case of no wind fires or in the absence of propagation mechanisms other than heat transfer by convection and radiation 74 75 between the flame front and the vegetation (by spot particles for example), because the sum of characteristic times associated with the physical process necessary for the 76 77 propagation of the fire (drying, pyrolysis, combustion ...) is larger than the travel time 78 characterizing the wind flow. Consequently, other approaches have been proposed to 79 improve the knowledge of the physical process responsible of the fire behavior. These 80 alternative class of fire models are based on more or less realistic description of the 81 physical phenomena governing the heat transfer between the fire front and the 82 vegetation [12]. A fully physical model addresses the problem of fire spread by analyzing 83 its behavior through its physicochemical aspects [13,14]. This approach minimizes the need of using an empirical parameterization, even if, compared to empirical and semi-84 empirical models, it needs bigger computational resources (which limit their capability 85 86 in solving the problem in real time), it is also more promising in the understanding of the 87 physics of fires [11, 15–18]. The fully physical approach has also a great potential in the 88 management of fire hazard in wildland urban interfaces, using an engineering approach, 89 such as the dimensioning of a fuel break, the evaluation of heat flux on a target located 90 inside the WUI, the interaction between two fire fronts [19–22].

91 The 3D model described in this work is based on a multiphase formulation and solves the 92 conservation equations of the coupled system formed by the vegetation and the 93 surrounding gaseous medium [13,18,23]. The model takes into account the vegetation

94 degradation processes (drying, pyrolysis, and combustion), the interaction between the 95 atmospheric boundary layer and vegetation (aerodynamic drag, heat transfer by 96 convection and radiation, and mass transfer), and the transport in the gaseous phase 97 (convection, turbulence, and combustion). The model is implemented in a modular and 98 parallelized 3D computation code referred to as "FireStar3D". The code is based on a 99 finite volume discretization of the governing transport equations (3rd order in time and 100 2nd order in space) and has undergone numerous validations [23–26]. The predictive potential of FireStar3D model was tested at a small scale in the case of litter fires (fire 101 102 propagation through a homogeneous fuelbed in a wind tunnel) [23]. The objective of this 103 study is to extend the tests at a larger scale for grassland fires. Grassfires have the great advantage to have been extensively studied experimentally, in very good conditions, 104 105 especially the experimental campaigns carried out in Australia [27-29], which are 106 considered as a good benchmark to test wildfire physical models [15,16,30]. For different wind speeds, fire behavior and spread through homogeneous grassland is analyzed in 107 108 terms of rate of fire spread, fire intensity, and shape of the fire front. The results were 109 compared with data collected during experimental campaigns and predictions from semi-110 empirical and other physical models.

111 **2. Modeling and Numerical Method**

112 The mathematical model is based on a multiphase formulation, it consists in a first step of averaging the conservation equations (mass, momentum, energy ...) governing the 113 114 behavior of the coupled system formed by the vegetation and the surrounding 115 atmosphere inside elementary control volumes including both the solid phase (the 116 vegetation) and the gaseous phase. This first operation, similar to a homogenization step, results in the introduction of source/sink terms on the right hand side of the equations, 117 representing the contributions of the interaction terms (exchanges of mass, drag, heat 118 119 flux ...) between the gaseous phase and the vegetation. The details of the model have been widely presented in previous publications, we invite the reader to consult references 120 121 [13,14,17,18,30] for more information. 122 The model consists of two parts that are solved on two distinct grids. The first part

- The model consists of two parts that are solved on two distinct grids. The first part consists of the equations of a reacting turbulent flow in the gaseous phase composed as a mixture of fresh air with the gaseous products resulting from the degradation of the solid phase (by drying, pyrolysis, and heterogeneous combustion) and the homogeneous combustion in the flaming zone. The second part consists of the equations governing the state and the composition of the solid phase subjected to an intense heat flux coming from the flaming zone.
- 129 Solving the gaseous phase model consists in the resolution of conservation equations of 130 mass, momentum, energy (in enthalpy formulation), and chemical species $(0_2, N_2, C0, N_2, C0)$ 131 CO₂, and H₂O) filtered using an unsteady RANS approach (TRANS) with Favre average 132 formulation [31]. The closure of the averaged conservation equations are based on the 133 concept of eddy viscosity [32] obtained from an evaluation of the turbulent kinetic energy 134 *k* and its dissipation rate ε. A high Reynolds number version of a two-equation statistical 135 turbulence model $(k-\varepsilon)$ is used with the RNG formalism [33,34]. The temperature dependence of the gas-mixture enthalpy is based on CHEMKIN thermodynamic tables 136 137 [35]. A combustion model based on Eddy Dissipation Concept (EDC) [32,36] is used to evaluate the combustion rate occurring in the gaseous phase. Finally, because radiation 138 heat transfer (mainly due to the presence of soot particles in the flame) plays an 139 140 important role for the propagation of the fire front, the field of soot volume-fraction in

141 the gas mixture is calculated by solving a transport equation [37,38] including a

thermophoretic contribution in the convective term and taking into consideration sootoxidation [39].

Concerning the solid phase model, during the thermal degradation, the composition of 144 145 the solid fuel particles representing the vegetation is represented as a mixture of dry 146 material (generic term for a mixing of cellulose, hemicellulose, and lignin), charcoal, 147 moisture, and residual ashes. For each solid particle, the model consists in solving the 148 equations governing the time evolutions of the mass fractions of water, of dry material, 149 of charcoal, as well as of the total mass of the solid particle, its volume fraction and its 150 temperature (the model does not assume a thermodynamics equilibrium between the gas 151 mixture and solid fuel particles). The degradation of the vegetation is governed by three 152 temperature-dependent mechanisms: drying, pyrolysis, and charcoal combustion. The 153 pyrolysis process starts once the drying process is completed and charcoal combustion 154 starts once the pyrolysis process is achieved. The constants of the model associated with 155 the charcoal combustion (activation energy and pre-exponential factor) are evaluated 156 empirically from a thermal analysis conducted on various solid fuels samples [13,40].

157 The interaction between the gaseous phase and the solid one is taken into account 158 through coupling terms that appear in both parts of the model. The coupling in the 159 momentum and turbulence equations is obtained by adding aerodynamic drag terms. These terms (both source and sink) are proportional to V (for turbulence destruction), to 160 V^2 (for the momentum equation), and to V^3 (for turbulence production), where V is the 161 local average of the velocity magnitude [30], and include a drag coefficient (evaluated 162 empirically) multiplied by a reference surface, defined here as the Leaf Area Density 163 (LAD). Heat transfer between the gas mixture and the solid fuel is based on empirical 164 165 correlations for convective transfer coefficient [40], and on the resolution of the radiative 166 transfer equation [41] that accounts for the presence of soot in the flaming zone and for the presence of hot particles in the vegetation layer (embers) [13]. Finally, mass transfer 167 from the solid phase to the gaseous phase is represented by adding source/sink terms in 168 169 the mass conservation equations of both phases.

170 The balance equations in the gaseous phase are solved numerically using a fully implicit 171 finite volume method in a segregated formulation [42]. "FireStar3D" model predicts turbulent reacting flows in rectangular domains using a structured but non-uniform 172 173 staggered mesh. Time discretization relies on a third order Euler scheme with variable time stepping strategy. To ensure numerical stability, space discretization is based on 174 175 second order schemes with flux limiters (QUICK scheme [43,44]) for convective terms 176 while diffusion terms are approached by central difference approximation with deferred 177 corrections [45] to maintain the second order accuracy in space. The Radiative Transport 178 Equation (RTE) is solved using a Discrete Ordinate Method (DOM), consisting in solving 179 the radiation-intensity equation in a finite number of directions [46]. The radiative 180 transfer equation accounts for gas-soot mixture absorption of radiative intensity 181 depending on the amounts of combustion products (CO_2 and H_2O), on the gas mixture 182 temperature, and of the soot volume fraction [47]. This set of discrete contributions is 183 then integrated using a numerical Gaussian quadrature rule (a S8 method is used) for the 184 calculation of the total irradiance. The set of ordinary differential equations describing 185 the time evolution of solid-fuel state (mass, temperature, and composition) are solved 186 separately using a fourth order Runge-Kutta method. From implementation point of view, 187 the computation code is parallelized [48] and optimized [49] using OpenMP directives 188 (operational on shared memory platforms and on Intel Xeon Phi coprocessors). Finally,

the hydrodynamic module of the code has been extensively validated on several
benchmarks of laminar and turbulent natural convection, forced convection, and
neutrally stratified flow within and above a sparse forest canopy [48–50].

Compared to the two main physical wildfire models referenced in the literature, i.e. WFDS 192 193 [15] and FIRETEC [16], FireStar3D shares many similitudes with WFDS but it also 194 presents important differences. In FireStar3D, as in WFDS, the flow solver is based on a 195 low Mach number formulation, a real calculation of the turbulent combustion in the flame 196 (using Eddy Dissipation Concept model), which is not the case in FIRETEC [30]. From a 197 numerical point of view, FireStar3D is fully implicit whereas the solver in WFDS is 198 explicit. One of the main differences at the modeling level with WFDS is related to the 199 estimation of the radiation heat transfer from the flame. In WFDS, the radiative heat 200 transfer is calculated but a minimum threshold value is fixed as a minimum radiative ratio 201 from the energy released from homogeneous combustion; this arbitrary approach was 202 not introduced in FireStar3D. These two characteristics, constitutes an important 203 progress toward a more physical wildfire model, it represents also a great challenge in 204 terms of computational resources.

205 **3. Grassland Fire Configuration**

As mentioned in introduction, the aim of this work is to show that the model is able to 206 207 predict numerically the spread of a fire through grassland. A perspective view of the 208 domain is shown in Fig. 1; the computational domain was 120 m long, 140 m wide, and 209 40 m high. The homogeneous vegetation layer, of height δ = 0.7 m, is 100 m long and 100 210 m wide, and it is located at 20 m from the domain inlet and at 20 m from the domain 211 lateral boundaries. The main physical characteristics of the vegetation layer are given in 212 Tab. 1. The heat yield of the fuel is 18000 kJ/kg, the solid fuel particles are assumed to 213 behave as a black body, and a vegetation family of cylindrical shape was considered. The 214 shape of the fuel particles is used for the description of their regression law and for the 215 estimation of the heat transfer coefficient. For the solid phase, a uniform grid with (Δx , 216 Δy , Δz) = (0.25 m, 0.25 m, 0.035 m) was used matching the vegetation zone, while a nonuniform grid of 224×248×90 cells was used for the fluid phase covering the whole 217 218 computational domain. Within the vegetation zone, the fluid-phase grid was uniform with 219 $(\Delta x, \Delta y, \Delta z) = (0.5 \text{ m}, 0.5 \text{ m}, 0.07 \text{ m})$ and then it was coarsened gradually toward the open 220 boundaries according to a geometric progression with common ratio 1.05. Both the solidphase and the fluid-phase grids were characterized by cells sizes below the extinction 221 222 length scale [14] within the vegetation given by $4/\alpha\sigma$ and equal to 0.5 m in our case. This 223 value should not to be exceeded in order to avoid fire extinction especially in the case 224 radiation-dominated fire propagation (i.e. when the wind speed is low to moderate). 225 Furthermore, in the context of using a high Reynolds number turbulence model, the 226 choice of the mesh size at the vicinity of solid bottom wall is strongly related to the quality of the obtained solution. The dimensionless distance to the wall z^{+} is defined by Eq. 1 227 where $C_{\mu} = 0.0845$, k is the turbulent kinetic energy, and ρ and μ respectively the density 228 and the dynamic viscosity of gas mixture. The center of any cell adjacent to the bottom 229 wall must have a dimensionless distance to the wall that satisfies the constraint 230 231 $11.5 < z^{+} < 500$ [44] (i.e. the cell center lies within the fully turbulent zone), and this 232 during the entire simulation time.

233
$$z^{+} = \frac{\rho C_{\mu}^{\frac{1}{4}} k^{\frac{1}{2}} z}{\mu}$$
(1)



234

Figure 1. Perspective view showing the dimensions of the computational domain and of the vegetation cover. The ignition line is 2 m wide and 50 m long. In the non-uniform ignition mode, the burner is activated from the middle of the ignition line toward its ends at the speed of 1 m/s.

239

Burner activation occurs at time t = 10 s, time for which the flow had reached a 240 241 statistically-steady state, this phase was considered for the entire cases studied in this 242 paper. During this (purely dynamic) flow settlement phase, homogeneous Neumann 243 boundary conditions were imposed at the open boundaries of the computational domain for all primary variables of the problem excepted for *v* and *z*-velocity components where 244 245 Dirichlet conditions (value set to zero) were imposed. In addition, a negative pressure 246 gradient is applied in the wind direction (*Ox*); this pressure gradient was automatically 247 adjusted during the flow settlement phase to obtain the desired level of the 10-m open wind speed. This procedure allowed collecting the turbulent fields at the open 248 249 boundaries, and these fields were then used during the burning phase, in particular for 250 the management of the entering turbulent fluxes.

251

Vegetation height δ	Solid-fuel volume-fraction α	Surface/ Volume ratio σ	Dry material density ρ	Moisture content <i>M</i>	Heat yield	Thermal emissivity	Vegetation family shape
(<i>m</i>)	C	(m ⁻¹)	(kg/m³)	(%)	(kJ/kg)		
0.7	0.002	4000	500	5	18000	1	Cylindrical

²⁵²

Table 1. Geometric and physical properties of the grassland vegetation [16,30]

At time t = 10 s, the burner was activated along an ignition line, extends over w = 50 m of length and 2 m of wide, as shown in Fig. 1. Fire was set by injecting CO gas at 1600 K in the burning zone from the bottom boundary of the domain. At time t = 10 s, the average velocity V_{inj} of CO was maximum (equal to 0.1 m/s), and then it was decreased linearly with the consumed mass of solid-fuel according to equation (2). This procedure avoided destabilizing the flame front by abruptly ceasing the CO injection and avoided any excessive external energy input.

261
$$V_{inj} = \left(I - \frac{m_b}{m_{b0}}\right) \times \left(0.1 \text{ m/s}\right)$$
(2)

In Eq. 2, m_{b0} represented the mass of dry material initially available above the burner area (i.e. the mass of dry material contained in the volume $V_{b0} = 2 \times 50 \times \delta$ m³). Equation 2 was used between t = 10 s and t = 35 s (i.e. during 25 s) as long as V_{inj} remained positive and CO injection ceased if V_{inj} reached zero during this time interval.

266

267 The parametric study focused on the influence of 10-m open wind speed on the fire behavior in terms of rate of spread, of fire intensity, and of shape of the fire front. The 268 269 simulations were carried out for six values of the 10-m open wind speed: 1, 3, 5, 8, 10, 270 and 12 m/s. These velocities were measured at the domain inlet, 10 m above ground. Two 271 modes of fire ignition were considered: uniform and non-uniform, for the entire range of the wind speed U. In the uniform ignition mode, the burner was activated at the same 272 273 time throughout the ignition zone. In the case of non-uniform ignition, the burner was 274 activated from the middle of the ignition line (at y = 70 m) toward its two end sides (at y 275 = 70 ± 25 m) at the speed of 1 m/s.

276

The results presented in this study were obtained using a variable time step strategy based on the truncation-error control, with time step values varying between 0.001 s and 0.01 s. At each time step, the solution is assumed to be obtained when the residuals of all conservation equations had reached 10⁻⁴ in normalized form. As a rough estimation of the computational cost, the simulation of 1s of fire propagation required about 7h of CPU time on a 28-cores node.

283 4. Numerical Results

284 This numerical study focuses on fire spread through a grassland whose vegetation structure is quite homogeneous (see Fig. 2) and identical to a natural undisturbed 285 286 grassland. The simulations were carried out under conditions similar to those of the Australian experimental campaign of 1986 [27–29]. The chosen configuration is very 287 288 similar to experiment C064 of controlled fire conducted by Cheney et al. (1986) on a 289 parcel of carefully cut grass [28] and shown in Fig. 3. However, the simulations were 290 carried out for tall grass ($\delta = 0.7$ m) unlike experiment C064 ($\delta = 0.21$ m); this choice was 291 mainly motivated by the existence of prior numerical studies [16,30]. In order to assess 292 the predictive potential of the model, the results were compared to the predictions of the 293 Australian empirical model MK5 [51], of the US semi-empirical model BEHAVE [52], of 294 three-dimensional physical models (FIRETEC from LANL and WFDS from NIST), and of a 295 two-dimensional physical model (FireStar2D [30]) that solved the problem of fire spread 296 in a vertical plane perpendicular to an infinite ignition line.



Figure 2. Structure of the grassland vegetation (tall-grass) (from https://commons.wikimedia.org/wiki/File:Dry_Grass.JPG)



301

Figure 3. Photos of experiment 'C064 - AU Grassland Fire' carried out by Cheney et al. [28], 27s (left) and 53s (right) after fire ignition starts. Vegetation layer height $\delta = 0.21$ m, fuel load $\alpha \rho \delta = 0.28$ kg/m², fuel surface/volume ratio $\sigma = 9770$ m⁻¹, moisture content *M* = 6.3%, ignition-line length w = 50 m, wind speed U = 4.6 m/s.

306

307 4.1. Fire Regimes and Fire-Front Shape

308 For a wind speed of 5 m/s, Fig. 4 shows a top view of the propagation of a grassland fire uniformly ignited at time t = 10 s (in a 2 m-wide and 50 m-long strip). Time t = 35 s 309 310 corresponds to end of ignition, unless the velocity of CO injection given by Eq. 1 had 311 reached zero before that time. The pyrolysis front used to evaluate the ROS can be clearly 312 seen on the mass fraction of the dry material. The results show: (i) the lateral fire spread 313 in addition to the propagation in the wind direction, (ii) the ripple effect on the sides of 314 the vegetation layer (visible at t = 55 s and t = 75 s) when the pyrolysis front reaches 315 these boundaries, and this effect becomes more visible with time (with more developed

316 ripples), (iii) the remote heating effect due to radiation, which is responsible for the drying of the fuel prior to arrival of the fire front, and (iv) the presence of some charcoal 317 downstream the ignition line that continues burning behind the fire front due to the 318 319 screening effect of CO injection that prevents the combustion of a part of charcoal 320 downstream the ignition line. With time, we notice that the fire front loses gradually its 321 parabolic shape and its forward-propagation speed becomes more important at the 322 lateral sides than at the central part of the fire front. However, the leading point of the 323 fire front remains nevertheless at the central part during the entire simulation. This effect 324 is not only inherent to the ignition method but also to the ratio between the length of the 325 ignition line and the lateral extent of the vegetation cover. Decreasing significantly this ratio should reduce this effect or might suppress it completely. Figure 5 is the counterpart 326 327 of Fig. 4 using the non-uniform ignition mode. The idea is to represent the ignition 328 method of experience C064, and more generally that of the Australian experimental campaign, where fire is set by two persons using a torch starting at the middle of the 329 330 ignition line and walking in opposite direction at the speed of 1 m/s. Testing this ignition 331 mode was motivated by the investigation of the parabolic shape of the fire front observed 332 experimentally, as shown by Fig. 3 and as confirmed by other experiments, despite the 333 observed loss of symmetry due to a change in the wind direction [28]. Other numerical 334 simulations obtained using the same kind of fire physical model, have exhibited similar 335 behavior, i.e. by igniting fire instantaneously along a sufficiently long width, the fire front 336 keep a nearly linear shape (slightly incurved toward the back) in its central part [15]. A 337 nearly parabolic front shape could only be reproduced numerically, if the ignition was 338 restricted to a quite small line (less than 10m) or using a dynamical ignition procedure 339 as in this study. Figure 5 shows in this case that the pyrolysis front is qualitatively more 340 consistent with the experimental observations. It seems however that the ROS value 341 (evaluated from the trajectory of the heading fire) is not significantly affected by the 342 ignition method. This was certainly due to the fact that the initial width of the ignition 343 line (50 m) was sufficiently long to not affect much the magnitude of the rate of spread. 344 Experimental investigations have shown that above an ignition line equal to 50 m the rate 345 of spread of the head fire was nearly equal to the theoretical value observed for an 346 infinitively long fire front [28]. We can notice on both simulations, that the lateral expansion of the fire front (flank fire) was correctly reproduced, this is a good indicator 347 348 of the quality of the model part in charge of the radiation heat transfer between the flame and the vegetation. This behavior was also correctly reproduced by simulations 349 350 performed using WFDS, whereas it was underlined as one of the major point to improve 351 in FIRETEC [16,53]. Figure 6 shows vertical profiles of primary variables at a duly chosen 352 location corresponding approximately to the furthermost point of the fire front in Fig. 5 353 (at t = 35 s). The figure highlights the appropriate mesh resolution for the evaluation of 354 the resolved-variables gradients and the production of the turbulent kinetic energy at the 355 surface of the fuel bed. To illustrate the remote heating effect mentioned earlier, figure 7 shows that the solid-fuel temperature at the fuel-bed surface exceeds that of the gas 356 357 mixture ahead of the fire front (located from the mass fraction of dry material). This means that the increase of the solid-fuel temperature is not the result convection heat 358 359 transfer from the gas mixture. Consequently and as mentioned before, this remote heating can only be imputed to radiative heat transfer from the flaming zone, resulting in 360 361 the water content loss observed ahead of the fire front in Fig. 7.



Figure 4. Top views of the computational domain (see Fig. 1) showing the propagation of a grassland fire in the case of a uniform fire-ignition mode (ignition at t = 10 s), for a 10-m open wind speed U₁₀ = 5 m/s. Left: mass fraction of dry material at vegetation height showing the shape of the pyrolysis front, right: temperature field (in Kelvin) at the surface of the solid fuel.

370



Figure 5. Top views of the computational domain (see Fig. 1) showing the propagation of a grassland fire in the case of a non-uniform fire-ignition mode (ignition at t = 10 s), for a 10-m open wind speed U₁₀ = 5 m/s. Left: mass fraction of dry material at vegetation height showing the shape of the pyrolysis front, right: temperature field (in Kelvin) at the surface of the solid fuel.

- 379
- 380
- 381



Figure 6. Vertical profiles of *u* and *w* (*x* and *z* components of the velocity), *k* (turbulent kinetic energy), and T_G (gas mixture temperature) obtained for $U_{10} = 5$ m/s, in the case of a non-uniform fire-ignition, at *t* = 35 s along line (*y* = 70 m, *x* = 32.6 m).

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387

Figure 7. Temperature difference between the solid fuel and the gas mixture, dry material and water mass fractions along the line (y = 70 m and $z = \delta$) obtained at t = 35 s, for a 10-m open wind speed U₁₀ = 5 m/s, in the case of a non-uniform fire-ignition mode.

3D views of the fire propagation obtained for a wind speed $U_{10} = 5 \text{ m/s}$ and a non-uniform ignition mode are represented in Fig. 8. These figures are taken at two characteristic times before and when the fire front had reached the side limits of the plot. These results show clearly the potential of FireStar3D in reproducing numerically (at least qualitatively) the propagation of the fire through a grassland. The model is able to reproduce the characteristic parabolic shape of the fire front associated with this type of ignition procedure (see Fig. 3) as it was mentioned in experiments on the field [15,28].



401

402 **Figure 8**. 3D View of one isovalue surface of the soot volume fraction (10^{-6}) colored by 403 the temperature of the gas (in yellow) and one isovalue surface of the water mass fraction 404 (10^{-3}) (in grey with 50% of transparency) for U₁₀ = 5 m/s and at different times, showing 405 the fire propagation in the case of non-uniform fire-ignition mode.

- 405 the fire propagation in the case of h 406
- 407

408 To understand the effect of the wind speed on the flame structure and more generally on 409 the dynamic of fire, 3D views of the fire propagation obtained for two extreme wind speed $U_{10} = 1$ m/s and 10 m/s are shown in Fig. 9. It is obvious that for a small value of the wind 410 speed ($U_{10} = 1 \text{ m/s}$), the flame plumes rise is not noticeably affected by the action of the 411 412 cross wind. In this case the fire front can be assimilated to an obstacle, and the air flow is deflected vertically by the plume. On the other hand, Fig. 9 shows how larger value of 413 wind speed ($U_{10} = 10 \text{ m/s}$) affects more significantly the rise of the flame plumes by 414 crossing the fire front and pushing the hot gases toward the unburned vegetation. We can 415 416 also notice that the wind speed increases significantly the depth of the fire front.



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Figure 9. 3D View of one isovalue surface of the soot volume fraction (10^{-6}) colored by the temperature of the gas (in yellow) and one isovalue surface of the water mass fraction (10^{-3}) (in grey with 50% of transparency) for U₁₀ = 1 m/s (top) and U₁₀ = 10 m/s (bottom), showing the effect of wind speed on the fire dynamics in the case of non-uniform fire-

423 ignition mode.

424

425 These phenomena are further illustrated by Fig. 10 showing cuts of the temperature and 426 the flow fields (streamline) in the vertical median plane. For moderate wind conditions, we notice that the fresh air is sucked from the vicinity of the fire front supplying the 427 428 thermal plume; the streamlines in Fig. 10 (top) show clearly the existence of aspiration 429 regions ahead the fire front. In the literature, this regime is often referred to as "plume 430 dominated fires". As indicated previously, these results highlight the capability of the 431 code to reproduce the backflow generated by the fire front on the leeward direction. In return for stronger wind conditions, the structure of the air flow is less affected by the 432 fire front as shown in Fig. 10 (bottom), and this effect is limited to the local acceleration 433 434 of the flow (resulting from a local expansion of the gas) in the plume and this regime is often referred to as "wind-driven fires". The streamlines show clearly the possibility for 435

436 the inlet air flow to cross the fire front. For this interaction between the fire and the flow 437 to be possible, the fire front must be structured vertically in peaks and troughs [54]. The reproduction of this configuration is not possible in 2D, because in 2D the fire front 438 439 represents a uniform thermal barrier. This justifies the interest in analyzing the behavior of the fire using 3D simulations, even if much greater computational resources are 440 441 required in this case. The interaction between the flames and the flow structures greatly 442 affects heat transfer ahead of the fire front and, consequently fire propagation; this is clearly illustrated by Fig. 11. We notice that in the case of a "plume dominated fire" (U = 443 444 1 m/s), radiative heat transfer prevails ahead of the fire front, indeed the temperature of the solid-fuel at the fuel-bed surface exceeds everywhere that of the gas mixture, and this 445 temperature difference decreases uniformly with the distance from the flaming zone. In 446 return, in the case of a "wind-driven fire" (U = 10 m/s), the fluctuations of this 447 448 temperature difference about zero is a clear signature of a prevailing convection heat 449 transfer between the gas mixture and the fuel bed.





451

452

Figure 10. Temperature field and streamlines of the gaseous phase, obtained in the vertical median plane (y = 70m) for $U_{10} = 1 m/s$ (top) and $U_{10} = 10 m/s$ (bottom), showing the effect of wind speed on the fire dynamics in the case of non-uniform fire-ignition mode.

457

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Figure 11. Temperature difference between the solid fuel and the gas mixture along the line (y = 70 m and $z = \delta$) ahead of the fire front, obtained in the case of a non-uniform fireignition mode for two different 10-m open wind speeds : U₁₀ = 1 m/s (at t = 80 s) and U₁₀ = 10 m/s (at t = 40 s), which corresponds to the temperature fields shown in Fig. 10.

To show the effect of wind speed on the flow structures, figure 12 shows, for two different 465 466 wind speeds (1 and 10 m/s) and in the case of a non-uniform fire-ignition mode, isovalue 467 surfaces of the *Q*-criterion colored by the vertical component of the velocity vector. This 468 invariant of velocity gradient tensor represents the balance between the rotation and strain rates. The *Q*-criterion is an appropriate tool for the visualization of turbulent eddy 469 470 formation, this criterion was introduced by Hunt et al. in 1988 [55]. The Q iso-surfaces 471 are good indicators of coherent structures in a turbulent flow, this variable is defined as 472 follows:

473

$$Q = \frac{1}{8} \left[\left(\frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right)^2 - \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)^2 \right]$$
(3)

474 where u_i is the velocity component in direction x_i . In addition of showing the three-475 dimensional nature of the flow, this figure highlights the flow structures present during 476 a grassland fire. This figure clearly shows that the assumption of a homogeneous plane 477 made for the fire front in the radiant panel theory is not valid, the fire front is structured 478 as a succession of peaks and troughs allowing for the air flow to find a way across it [54]. 479 This heterogeneity of the flame and the flow structure along the transverse direction, 480 which is a great demonstration of 3D effects in a fire, affects a lot the propagation of the fire, as it has been clearly demonstrated experimentally at small scale [56] and 481 numerically at larger scale [57]. The main effect is that, when the wind flow is able to 482 483 cross the fire front, recirculating zones are formed at the back of the fire front, which 484 redresses the flame and affects significantly the heat transfer between the flame and the vegetation and therefore the rate of spread. This effect is only visible above a certain 485 486 threshold value of the wind speed. Being able to capture these flow details using an 487 unsteady RANS approach is due to a relatively fine mesh resolution matching the 488 extinction length scale $(4/\alpha\sigma)$ characterizing the absorption of the radiation inside the

- 489 vegetation layer. This leads us to possibly consider a fully Large Eddy Simulation (LES)
- 490 approach using a comparable mesh resolution (that seems to be sufficient to capture the
- 491 flow coherent structures), where a transport equation of the turbulent kinetic energy k
- 492 only needs to be solved (instead of the two-equation k- ε model).
- 493





496 **Figure 12.** Flow structure in a grassland fire for two 10-m open wind speed $U_{10} = 1$ m/s 497 (top) and $U_{10} = 10$ m/s (bottom) and for a non-uniform fire-ignition mode, shown using 498 an isovalue surface of the *Q* criterion ($Q = 0.5 \text{ s}^{-2}$) colored by the vertical component of 499 the velocity field.

500

501 **4.2. Rate of Fire Spread**

502 To go further in the analysis, we consider now two quantitative parameters, 503 characterizing the fire: the Rate Of Spread (ROS) and the intensity of the fireline. The 504 evolution of the ROS with the 10-m open wind speed (U_{10}) is shown by Fig. 13. The ROS estimation was obtained from the time derivative of the position of the pyrolysis front at the surface of the vegetation cover. Because this operation needs a certain level of regularity of the concerned curve, it was carried out in the vertical median plane (i.e. along the line y = 70 m, $z = \delta$). Since the ignition procedure was initiated from the center to the sides, the head fire was always located in the median plane. Therefore this value can be considered to the same value of the rate of spread of the head fire, where the ROS reached its maximum value.

512



513

Figure 13. Rate of fire spread (ROS) through a uniform grassland obtained for different 10-m open wind speeds. The results of this study (FireStar3D) are compared to the results obtained experimentally (Cheney et al 1993, 1995, 1998 [27-29]), and using an empirical model (MK5 [8]), a semi-empirical model (BEHAVE [10]), 3D numerical models (FIRETEC [16], WFDS [15, 20]), and a 2D numerical model (FireStar2D [30]).

519

The experimental data shown in Fig. 13 were obtained from Cheney et al. [27-29] for 520 521 different lengths w of the ignition line. These experimental studies show that the ROS 522 increases with *w*, as found by FIRETEC model predictions (16 m and 100 m) [16], before 523 reaching an asymptotic value for *w* > 200 m. For example, when *w* increased from 50 m to 250 m, the ROS increased by about 30% for $U_{10} = 3$ m/s and 6 m/s. The authors 524 reported that this scale effect was more pronounced for larger wind speeds. Concerning 525 526 the relatively large dispersion of the experimental measurements, it can result from the 527 unsteadiness nature of the wind flow [58]. On the other hand, the reported experimental 528 data for $U_{10} \ge 8$ m/s [29] were estimated from measurements recorded during real wildfires with significantly large fire front (the ROS reaches its maximum value) but for 529 530 which wind speed and vegetation characteristics are not under control as in experimental 531 fires. We recall that the simulations were carried out under conditions similar to those of 532 experiment C064 conducted by Cheney et al. [28]. The main difference lies in the grass 533 height ($\delta = 0.7$ m in the simulations compared to $\delta = 0.21$ m for experiment C064) and

534 this choice was mainly motivated by the existence of prior numerical studies [16,30]. For 535 low to moderate U_{10} values (up to 6 m/s), FireStar3D results compare well with 536 experimental data and with other predictions, and we can observe a quasi-linear 537 evolution of the ROS. Between 1 and 5 m/s we can notice a less influence of the wind 538 speed upon the rate of spread, this result is compatible with the transition between a 539 plume dominated fire (for $U_{10} = 1 \text{ m/s}$) and a wind driven fire ($U_{10} = 5 \text{ m/s}$)[58,59]. For 540 these values of wind speed, a steady regime of fire propagation was clearly reached in the 541 simulations, as shown by Fig. 14 for $U_{10} = 1 \text{ m/s}$ from the regular and constant slop of the 542 fire front position versus time. For $U_{10} = 8$ m/s, the results are consistent with the 543 predictions of other models and with the experiments, despite the relative dispersion of 544 the experimental measurements which prevents a significant comparison. For $U_{10} \ge 10$ 545 m/s, FireStar3D clearly underestimates the ROS (just as FIRETEC and WFDS do) mainly because of the short ignition-line length of 50 m that has been considered and also 546 547 because of the longitudinal extension of the plot (100 m) which were too short to reach quasi-steady conditions of propagation, as shown by Fig. 14 for $U_{10} = 10$ m/s from the 548 549 highly irregular evolution of the fire front position with time.

550



551

Figure 14. Position versus time of the furthermost point of the pyrolysis front at the fuelbed surface obtained in the case of a non-uniform fire-ignition mode for two different 10m open wind speeds : $U_{10} = 1 \text{ m/s}$ and $U_{10} = 10 \text{ m/s}$.

555

556 To illustrate further this last point, the results obtained with WFDS reported in Fig. 13, 557 were obtained with a plot 50 m long, with a consequence that the ROS seems to saturate 558 above a certain value of the wind speed (8 m/s). On the other hand, FireStar2D that 559 assumes a straight and infinite pyrolysis front better predicts the ROS at high wind speeds (10 m/s and 12 m/s). In return, 2D models fail to account for the aerodynamic drag on 560 561 the lateral border of the fire front that is primarily responsible for its curvature, which 562 results in the overestimation of the ROS at low to moderate wind speeds. Both for the 563 empirical model (MK5) and semi-empirical one (BEHAVE), the experimental fires that helped elaborating them could not be carried out properly for wind speeds exceeding the 564 threshold value of 7-8 m/s [10], leading to an underestimation of the ROS by these models 565 566 at high wind speeds. We can explain the discrepancies between MK5, BEHAVE and field

567 measurements by the fact that for safety reasons the experiments carried out to elaborate 568 the MK5 model cannot be conducted under strong wind conditions, whereas for BEHAVE 569 model there is a real scaling problem in extrapolating experimental data collected at 570 small scale in a wind-tunnel to fires at large scale such as in grassland.

572 **4.3. Fire Intensity**

571

573 The fireline intensity (I_{BYR}) at the center of the fire front (maximum value) can be 574 evaluated from Eq. 4 (Byram's intensity [60]), where $m = \alpha \rho \delta$ is the fuel load (equal to 0.7 575 kg/m² according to Tab. 1), and ΔH is the heat yield of the fuel (estimated at about 18000 576 kJ/kg [61]).

577
$$I_{BYR} = m \times \Delta H$$

578 Because this approximation is theoretically valid only for a straight front propagating at 579 the same speed, we have chosen to evaluate numerically the fireline intensity from the 580 Heat Release Rate (HRR) defined by Eq. 5 as the product of ΔH and the rate of total mass-581 loss of vegetation in the entire computational domain.

 $\times ROS$

582
$$I = \dot{m} \times \Delta H$$

(5)

(4)

The time evolution of the heat release rate, evaluated from Eq. 5 with $\Delta H = 18\ 000\ \text{kJ/kg}$, are shown in Fig. 15 (for three values of wind speed). The figure shows that the heat release rate grows until the lateral branch of the fire reach the limit of the plot, more or less at the same time (75 s) for these three values of the wind speed, mainly because the propagation of the flank fire is less affected by the air flow.



588

Figure 15. Time evolution of the Heat Release Rate (HRR) of the fire obtained from the rate of total mass-loss evaluated for the whole solid-fuel layer, in the case of non-uniform fire-ignition mode, for three different 10-m open wind speed $U_{10} = 1$, 5, and 10 m/s. For $U_{10} = 10$ m/s, the fire front reaches the end of the domain around t = 76 s.

The fireline intensity can be estimated numerically by dividing the average value of the heat release rate reached when the fire was fully developed (HRR_{∞}) by the width *w* of the plot (100 m) according to Eq. 6.

597
$$I \approx \frac{HRR_{\infty}}{W}$$
 (6)

598 Using the fire line intensity calculated from Eq. 6, it is then possible to evaluate Byram's 599 convective number N_c defined as the ratio between the buoyancy force and the inertial 600 force due to the wind [59] and given by Eq. 7, where *g* is the acceleration of gravity (9.81 601 m/s²), and ρ_0 (1.171 kg/m³) and C_{P0} (1010 J/kg.K)) are the density and the specific heat 602 of ambient air at temperature $T_0 = 300$ K.

603
$$N_C = \frac{2gI}{\rho_0 C_{P0} T_0 (U_{10} - ROS)^3}$$
(7)

Byram's convective number is an indicator of the fire propagation regime. Large values
of Byram's number are normally obtained in fires governed by plumes (plume dominated
fires), with a heat transfer between the flame and the vegetation dominated by radiation.
Whereas small values of Byram's number are obtained in fires piloted by inertial effects
(wind driven fire), with a more important contribution of the convection heat transfer
[14,59].

A comparison between the two methods of calculation of the fireline intensity (I_{BYR}) 610 611 obtained from Eq. 4 and *I* obtained successively from Eqs. 5 and 6) is presented in Tab. 2. 612 We can notice that the deviation between these two approaches increases with the wind 613 speed: for $U_{10} = 1$ m/s, the relative variation $\Delta I/I$ is equal to 26%, while for $U_{10} = 12$ m/s, $\Delta I/I$ is equal to 101%. Two factors can explain these differences: (1) in the calculation of 614 I_{BYR} the rate of spread was evaluated at the center of the front line (where the ROS was 615 maximum) and averaged over the propagation time of the fire; and (2) it was assumed 616 that all the solid fuel had burned. Both these effects result in an overestimation of the 617 quantity of fuel consumed by the fire and are therefore responsible for the 618 overestimation of I_{BYR} (as seen in Tab. 2). Furthermore, these effects become more 619 pronounced as the wind speed increases, which explains why the relative difference $\Delta I/I$ 620 621 was smaller for a wind speed of 1 m/s than for 12 m/s.

622

<i>U</i> ₁₀ (m/s)	1	3	5	8	10	12
I _{BYR} (kW/m)	8820	11340	15120	25200	31500	40320
<i>I</i> (kW/m)	7000	8000	14000	17000	19000	20000

623**Table 2.** Fireline intensity evaluated using two approaches: (1) from the average rate of624spread and assuming that the initial fuel load had fully burned (I_{BYR} , Eq. 4) and (2) from625the rate of total mass-loss of solid fuel (I, Eq. 6).

626

627 To illustrate the relation between Byram's convection number and the fire regime, we 628 notice for example that for a 10-m open wind speed $U_{10} = 1$ m/s, Byram's number N_c , 629 estimated from Eq. 7 using the value of the ROS from Fig. 14 and the value of *I* from Tab. 630 2, is about 14300, while for $U_{10} = 10$ m/s, N_c is about 2.5. We can conclude that the

631 situation observed for $U_{10} = 1$ m/s was clearly a plume dominated fire, and that for $U_{10} =$

632 10 m/s the situation was closer to a wind driven fire. The ratio ROS/U_{10} versus the 633 inverse of Byram's convective number N_c (calculated from Eq. 7) is shown in Fig. 16, 634 where the numerical results are compared to experimental data collected from the 635 various experimental campaigns carried out in Australia [27-29, 62]. Despite some discrepancies between numerical and experimental data, the two sets of data compare 636 relatively well. As pointed out in a previous study [17,58], the maximum value of the ratio 637 ROS/U_{10} (equal to 0.7 in our case) is obtained for fires dominated by buoyancy (plume 638 639 dominated fires), and thus for small values of the ratio $1/N_{\rm C}$. On the other side of the curve 640 (i.e. for large values of $1/N_{\rm C}$), the ratio ROS/U₁₀ tends towards a constant value (nearly 641 equal to 0.25). That means that for fires dominated by inertial forces (wind driven fires) the ROS converges toward a linear relationship with the wind speed. This behavior has 642 643 been reported by many experimental studies, in various ecosystems (surface fires in 644 grassland, shrubland ...) [62]. The relatively high values observed for the two branches of the curve (comparable to the values observed on the field), can be interpreted as a 645 consequence of the low value of the fuel moisture content (M = 5%) that contributes 646 647 significantly to promote the propagation of the fire, and therefore to obtain high rates of 648 spread.

649



650

651 **Figure 16.** Ratio ROS/U_{10} versus the inverse of Byram's convective number N_C, 652 comparison between numerical results and experimental data [62].

653 **5. Conclusions**

This study reported numerical simulations of fire spread through a homogeneous grassland. The results were obtained using a 3D Computational Fluid Dynamic code based on a fully-physical multiphase model. At low to moderate wind speeds (up to 8 m/s), the simulated Rate Of Spread of fire (ROS) was in good agreement with the data of the experimental campaign conducted in Australia, with the predictions of operational empirical models (such as MK5 and BEHAVE), and with 660 the numerical results of other 3D physical models (FIRETEC and WFDS). At high wind speeds (10 m/s and 12 m/s), a larger extends of the vegetation cover and a 661 larger length of the ignition-line would be required in order to reach the 662 asymptotic values of the ROS. Nevertheless, the results of FireStar3D were in good 663 agreement with the predictions of other 3D physical models (FIRETEC and WFDS). 664 The study has also shown that the method of fire ignition can affect significantly 665 the shape of the fire front without affecting significantly the rate of fire spread. 666 667 Consequently, it seems that the non-uniform fire-ignition of the grassland 668 (consistent with the experimental procedure) allows recovering the parabolic shape of the fire front observed experimentally. The analysis of the results by 669 exploiting the rate of total mass-loss of solid fuel has allowed to reconstruct the 670 evolution of the ratio ROS/U10 as a function of the inverse of Byram's convective 671 672 number. This parameter is a good indicator to highlight the existence of two propagation regimes of surface fires, namely the plume dominated and the wind 673 674 driven fires. The next step of this work, would be to explore the 3D interactions 675 between a quasi-infinite width fireline (reproduced using periodic conditions at 676 the lateral boundaries of the fuel layer) and the atmospheric boundary layer. 677 Various aspects of this problem could be studied, such as the impact of the 678 unsteady nature of the wind speed, the competition between the inertial forces and 679 buoyancy, the aerology generates by the fire itself, the coherent structures 680 observed along the fire front and their impact upon the fire dynamic. These aspects 681 would be better addressed using the new simplified LES model implemented in 682 FireStar3D. This model had been validated in the case of an isothermal flow 683 through homogenous and inhomogeneous canopies [25, 26], and has been recently 684 extended to account for fire propagation. Many other fundamental aspects of the 685 wildfire dynamic are not well understood, such as the role played by the field slope 686 (and the competition between the wind and the slope when their directions are not 687 aligned), the impact of the fuel moisture content (its threshold effect in the 688 burn/no burn process, the linear or exponential decay of the rate of spread ...). In 689 complement to experimental investigations, detailed physical models (such as 690 Firestar3D) could be good tools for the understanding of the basic physical 691 processes governing the behavior of wildfires. In more practical contexts, this kind 692 of numerical simulation tools can be used to analyze the effects of the vegetation 693 layer properties (heterogeneity, discontinuity ...) or to simulate some operational 694 situations, such as prescribed burning (to evaluate the thermal impact in the soil), 695 counter-fires ignited during firefighting operations [20], or to study the efficiency 696 of a fuel break [19].

697 Acknowledgements

This work was granted access to the HPC resources of Aix-Marseille Université funded by the project Equip@Meso (ANR-10-EQPX-29-01) of the program "Investissements d'Avenir" supervised by the "Agence Nationale pour la Recherche". The authors thank the anonymous reviewers for the quality of their analysis, their reports have contributed a lot to improve the paper.

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- Numerical simulations of grassland fire
- Detailed physical fire model
- Plume dominated fire, wind driven fire
- Byram's convective number